



## Experimental and Numerical Analysis of Ambient Crosswind Effects on a Floating Solar Chimney Power Plant Performance

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### A B S T R A C T

Floating solar chimney (FSC) power plant is a novel kind of solar thermal technologies which uses the buoyant airflow and chimney (stack) effect to make an artificial airflow and generate electricity from aero-turbines. Also FSC has the capability of economic competition with conventional and other renewable power plants. Considering the FSC structure, it is obvious that, ambient cross wind (ACW) has significant influence on the FSC performance. The main purpose of this study is an investigation on the effect of ACW on updraft airflow inside a FSC which is a considerable parameter on system performance. In addition, FSC operation has been analyzed at different tilt angles when exposed to external crosswind. Hence, a geometrical model consisting of FSC and its surrounding ambience is simulated and mathematical model is proposed to demonstrate the fluid flow, heat transfer and performance of entire system are further developed. The variation of FSC updraft velocity is analyzed in different ACW velocities. In this research, design and construction of a small-scale (laboratory model) floating solar chimney is performed and numerical results are verified with experimental setup data. Analysis of numerical simulation indicates that when the ACW is relatively weak, it will deteriorate the updraft air flow velocity of fixed solar chimney or vertical floating chimney due to the tip vortices effects. Increasing the tilt angle of the floating chimney causes a decrease in tip vortices formation and finally make a considerable improvement in updraft velocity compared to the fixed (vertical) chimney. Although inclination of the floating chimney decreases the physical height, the performance of FSC is better than fixed type due to the reduction of the tip vortices effect in windy conditions. The present work can be useful to predict the performance of large-scale FSC by considering the influence of ACW.

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### 1. Introduction

The solar updraft power plant system (SUPPS) is one of the modern renewable energy technologies which has the capability of economic competition in comparison with the conventional power plants. SUPPS harness and convert solar radiation to electrical energy by combination of the three well-known main parts. As shown in Fig. 1 SUPPS uses an open-solar-air collector to warm up entering air from ambient and makes buoyancy. The central chimney acts as a thermal engine and converts thermal energy to kinetic energy in flowing air inside the system. A portion of this kinetic energy is converted to electricity in aero-turbines that located in the base of chimney structure [1, 2]. The first SUPPS prototype was constructed in Manzanares, Spain in the early 1980s by Schlaich and his partners. This prototype consists of a solar collector with diameter of about 244m and 2m to 6m in height from inlet to center. The chimney has 194.6m in height and 20m in diameter. Manzanares power station operated with a peak output of 50 kW for over 7

years. After that, relevant researches on the SUPPS continued due to its prosperous future and considerable development occurred in numerical analysis and experimental prototype. Several research and industrial groups evaluate the possibilities of constructing SUPPS such as EnviroMission Company in Australia and in Arizona (USA) [3]. Based on Manzanares prototype, Pasumarthi and Sherif [4, 5] developed a comprehensive mathematical model to evaluate thermo-fluid analysis of SUPPS and they built small-scale SUPPS prototype to investigate the impact of miscellaneous parameters, such as geometrical dimensions and environmental conditions on thermo- fluid properties such as temperature, velocity and power output. They also examine several types of SUPPS prototype with consideration of the chimney shape, the collector construction in Florida in order to study on fluid flow and heat transfer of various scales of SUPPS [6]. Economic analysis and basic theory of large-scale SUPPS is presented by Schlaich et al which is utilized to design of a 200-MW

industrial-scale SUPPS [7]. Pretorius and Kröger presented a mathematical model to simulate SUPPS numerically and analyzed the influence of various calculating technique on output power [8]. Ming et al. studied and developed a thermodynamic model to investigate the performance of a SUPPS by evaluating the influence of different parameter on the relative pressure, driving force, power output and efficiency [9]. Also Zhou et al. performed different experimental investigation on mini- scale of SUPPSs [10]. Koonsrisuk and Chitsomboon modeled the operation of large scale SUPPSs by utilizing the dimensional analysis to obtain a dynamic similarity between its scaled models and prototypes [11, 12]. Zhou et al. investigated the impact of chimney height on the performance of SUPPS exposed to standard lapse rate of environment temperature [13]. Fluri et al. presented a detailed economic study on SUPPS [14]. Petela developed a simplified comprehensive mathematical model for SUPPS where 2nd law analysis has been used to determine and evaluation of exergy flow in the whole system [15]. The conventional solar chimney is usually built by reinforced concrete. Although it has a long life span, in order to generate sufficient buoyancy flow due to natural convection, the chimney height is required to be high enough which has creates some disadvantages such as high construction cost, restriction on the structure material and limited height due to the technological constraints. Also the natural event instant of possible earthquake can destroy very tall chimney easily as well as a cross wind produce vibration effects on the chimney structure. With increasing wind speed, a significant amplification of the cross flow forces occurs and large amplitude of cross flow oscillations is created which can destroy the solar tower [16]. Based on these facts, the idea of Floating Solar Chimney (FSC) technology was presented by Papageorgiou for the first time. The novelty of FSC technology is to avoid to major problems due to the ambient cross wind, heavy weight and the construction cost of solar chimney but its life span is shorter than rigid concrete solar chimneys. The FSC can be built for hundreds of meters without major considerations. It can be a significant improvement in power generation and omit the limitations of using of rigid concrete structure for solar chimney [17]. However, a precise attention on previous publications represent that scientific authors focused more on solar radiation effects rather than on the influence of ambient cross wind on SUPPS especially FSC. Existing research indicates that ambient cross wind causes very complex situation on SUPPS [18-20]. Up to now, few studies about the impact of ambient cross wind on the SUPPS have been carried out. Niemann et al. presented a model of SUPPS with consideration of cross wind in order to analyze the structural reliability of the high chimney [21]. Later, an analysis about structural dynamic aspects on the SUPPS was carried out by Borri et al [22]. Following that, Ming et al. studied the impact of ACW on the SUPPS operation through the collector inlet and chimney outlet. It is

found that an ACW affects the SUPPS in two ways. First, when the velocity of ambient cross wind is comparably low, it will degenerate the flow field and decrease the power generation of the SUPPS whereas if the ACW is strong enough, it may improve the updraft flow rate and SUPPS performance [1].

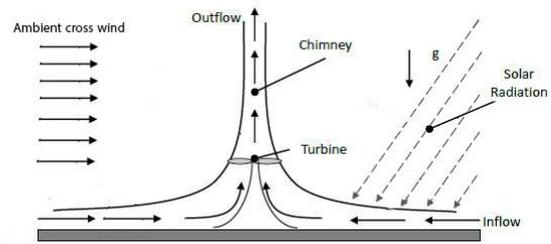


Figure 1. Schematic of solar chimney power plant and main parts

The objective of this paper is to investigate the effect of ACW on updraft air flow inside the FSC which is a considerable parameter on system performance. Hence, a numerical simulation is performed on geometrical FSC model in various tilt angels, when exposed to external crosswind. The numerical model is validated by small-scale FSC model which is designed and constructed by researcher group. Further, the influence of ACW on the chimney outlet is studied.

## 2. Materials and Methods

In this section, details of numerical modeling and experimental study are presented. In the field of numerical analysis, geometrical model, computational domain, mathematical model and governing equations and finally selected profile for simulating the ambient cross wind are discussed. Following that, the main steps of experimental study such as design, build and test of a floating solar chimney power plant laboratory model are described. Primary data obtained from lab model are used to validate the results of numerical solution. In order to realize the impact of ACW on entire FSC system, the model was located in the center of nonexistent cubical box as shown in Fig 2.

The chimney has 70 cm in height and 5.8 cm in diameter. The solar collector has 63 cm in diameter and the height from the ground surface is 4 cm. In Fig. 2, x-axis is aligned in velocity direction of the ACW and z-axis in the straight up direction. Assuming the symmetric property to be perpendicular to the y-axis direction, so a half system was considered in the model which is an acceptable assumption for steady state numerical solution. Thermal storage system is not considered in this study and numerical model uses equivalent ground heat flux produced by solar collector instead of global solar radiation. Considering the main objective of present work, ACW on updraft velocity inside

the chimney, radiation heat transfer is not necessary to evaluate [23].

Investigating fluid flow and heat transfer characteristics within the FSC and its ambience are actually complicated. In this research, pure natural convection produced by solar radiation (here equivalent ground heat flux) is the main governing flow physics for the floating solar chimney system when the ACW is absent.

The non-dimensional number that can measure the intensity of the buoyancy-induced flow is the Rayleigh number as defined below:

$$Ra = \frac{g\beta\Delta TL^3}{\nu\alpha} \quad (1)$$

where  $\Delta T$  is the maximum temperature increase within the FSC.  $\alpha$ ,  $\beta$  and  $L$  are the thermal diffusivity, thermal expansion coefficient and the collector height, respectively. However, the ACW plays considerable role in this study which causes the system to be combination of natural and forced convection. The non-dimensional number relates the influence of ACW to the whole FSC system and is represented as:

$$\frac{Gr}{Re^2} = \frac{\frac{g\beta\Delta TL^3}{\nu^2}}{\left(\frac{u_\infty L}{\nu}\right)^2} = \frac{g\beta\Delta TL}{u_\infty^2} \quad (3)$$

where,  $Gr$  and  $Re$  are Grashof and Reynolds numbers, respectively and  $u_\infty$  is the average ACW velocity imposed to FSC. In the collector, the fluid flow is much weaker than the chimney, so the flow region can be distinguished firstly according to dimensionless group numbers.

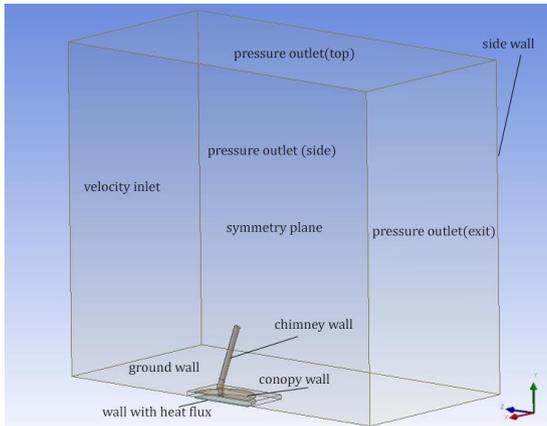


Figure 2. Computational domain for FSC numerical simulation and main boundary conditions

Preliminary analysis showed that the fluid flow within FSC is turbulent even though the velocity of ACW is zero. The presence of ACW will cause the flow to be more turbulent [24, 25]. So the turbulent model should be chosen to determine the fluid flow and heat transfer in the FSC for which both forced and natural convection was considered.

The Boussinesq approximation can be assumed for the buoyancy force in the momentum equation where the density variation is a linear function of temperature change in the collector. This assumption can only be implemented with small temperature differences [1]. Also, realizable  $k - \varepsilon$  turbulence model is selected throughout this research, and we propose that the flow is fully turbulent [26]. Governing equations for fluid flow, heat transfer and turbulent modeling can be written as follows:

Continuity:

$$\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u_i)}{\partial x_i} = 0 \quad (2)$$

Momentum:

$$\frac{\partial(\rho u_i)}{\partial t} + \frac{\partial(\rho u_i u_j)}{\partial x_j} = \rho g \beta (T - T_\infty) - \frac{\partial p}{\partial x_i} + \frac{\partial \tau_{ij}}{\partial x_j} \quad (3)$$

Energy:

$$\frac{\partial(\rho c_p T)}{\partial t} + \frac{\partial(\rho c_p u_j T)}{\partial x_j} = \frac{\partial}{\partial x_j} \left( \lambda \frac{\partial T}{\partial x_j} \right) - \tau_{ij} \frac{\partial u_i}{\partial x_j} + \beta T \left( \frac{\partial p}{\partial t} + u_j \frac{\partial p}{\partial x_j} \right) \quad (4)$$

Realizable turbulent kinetic energy:

$$\frac{\partial(\rho k)}{\partial t} + \frac{\partial(\rho k u_i)}{\partial x_i} = \frac{\partial}{\partial x_j} \left( \alpha_\varepsilon \mu_{eff-k} \frac{\partial k}{\partial x_j} \right) + G_k + G_b - \rho \varepsilon \quad (5)$$

Realizable turbulent energy dissipation:

$$\frac{\partial(\rho \varepsilon)}{\partial t} + \frac{\partial(\rho \varepsilon u_i)}{\partial x_i} = \frac{\partial}{\partial x_j} \left( \alpha_\varepsilon \mu_{eff-\varepsilon} \frac{\partial \varepsilon}{\partial x_j} \right) + \rho C_1 S_\varepsilon - \rho C_2 \frac{\varepsilon^2}{k + \sqrt{\nu \varepsilon}} + C_{1\varepsilon} \frac{\varepsilon}{k} C_{3\varepsilon} G_b \quad (6)$$

$$\mu_{eff-k} = \left( \mu + \frac{\mu_t}{\sigma_k} \right) \quad (7)$$

$$\mu_{eff-\varepsilon} = \left( \mu + \frac{\mu_t}{\sigma_\varepsilon} \right) \quad (8)$$

where  $G_k$  denotes the generation of turbulence kinetic energy caused by the mean velocity gradients and can be defined as:  $G_k = -\rho \overline{u_i' u_j'} \frac{\partial u_j}{\partial x_i}$  or  $G_k = \mu_t S^2$  where  $S$  is the modulus of the mean rate-of-strain tensor and described as:  $S = \sqrt{2S_{ij}S_{ij}}$ . The generation of turbulence kinetic energy

due to buoyancy,  $G_b$  is expressed as  $G_b = -g\beta \frac{\mu_t}{\rho \text{Pr}} \left( \frac{\partial T}{\partial x_i} \right)$

and the turbulent viscosity,  $\mu_t$  is defined as:  $\mu_t = \rho C_\mu \frac{k^2}{\varepsilon}$

where  $C_\mu$  is based on the mean rate of strain and rotation, the angular velocity, and the system rotation. The value of this constant is 0.09.  $\sigma_k$  and  $\sigma_\varepsilon$  show the turbulent Prandtl numbers for  $T$ ,  $k$  and  $\varepsilon$  respectively:  $\sigma_k = 1.0$ ,  $\sigma_\varepsilon = 1.3$ . In

addition  $c_1, c_2, c_{1\varepsilon}, c_{3\varepsilon}$  are constant for turbulent

$$\text{model: } c_{1\varepsilon} = 1.44, c_2 = 1.9, c_1 = \max \left[ 0.43, \left( S \frac{k}{\varepsilon} \right) / \left( S \frac{k}{\varepsilon} + 5 \right) \right]$$

$$\text{and } c_{1\varepsilon} = \tan \left| \frac{v}{u} \right|$$

which is a relationship between the velocity vector parallel and perpendicular to the gravitational vector. Both natural (buoyancy effect) and forced (ACW effect) convection have been considered, respectively, by the first and second terms of in the right side of momentum equation. If ACW is strong enough, forced convection will overcome the effect of natural convection and if ACW is weak, natural convection will dominate the forced convection and press. Force item can be neglected. The boundary condition for numerical simulation to investigate the influence of ACW on the whole system are represented in Table 1.

Table 1. boundary condition for numerical simulation

Faces	Boundary type	Value
Ambient inlet (x=0)	Velocity inlet	1.85 m/s
Ambient outlet	Press. outlet	0 pa
Ground surface (under canopy)	Heat flux	500-2080 W/m <sup>2</sup>
Ground surface (outside canopy)	Constant temperature	300 k
Chimney surface	Adiabatic wall	0 W/m <sup>2</sup>
Collector canopy surface	Wall	couple
Symmetry surface (y=0)	Symmetry	-

The wind speed profile can be described as the logarithmic function which is defined as:

$$u = A \ln(z / z_0), v = w = 0 \quad (10)$$

where A is a constant and z is the height. Also, is defined as aerodynamic roughness length of the ground. Ambient outlet contains 3 faces: the top surface of the model, the surface parallel to the ambient inlet surface and the surface parallel to the symmetry surface. Ambient inlet contains 3 faces: the top surface of the model, the surface parallel to the ambient inlet surface and the surface parallel to the symmetry surface. Also, the boundary condition for cubic box is shown briefly in Fig 2.

A simple lab scale experimental setup of a floating solar chimney is used in order to simulate real filed studies and validate numerical results. The main dimensions of experimental setup are the same as mentioned previously. Equivalent ground heat flux is achieved by using electrical heating elements. The quantity of heat flux is calculated by production of whole element voltage in current divided by collector area. Collector roof and chimney wall are made of transparent glass. 5 chimneys with different tilt angles 0, 10, 20, 30 and 35 degree are used instead of a flexible floating chimney. FSC setup is located in the test section of a low speed wind tunnel to evaluate the effect of ACW on the whole system. Free stream wind speed reaches 1.85 m/s

during the test and all the tests are performed in this speed. Voltage is regulated to generate ground heat fluxes in quantities of 500, 787, 1143, 1565 and 2080 W/m<sup>2</sup>. Experimental data from multi-meter, thermometer and turbine flow meter are captured after steady state condition is achieved. A view of experimental setup in wind tunnel is shown in Fig. 3.



Figure 3. Experimental setup for Floating Solar Chimney located at the test section of a low speed wind tunnel

### 3. Results & Discussion

At the beginning of this section, the distribution ambient cross wind produced by wind tunnel is shown in Fig. 4. Curve fitting on experimental data shows that the produced velocity profile obeys logarithmic profile in an acceptable match or, in other words, natural wind profile is simulated in wind tunnel test section.

Variation of updraft velocity and temperature difference in the collector versus input heat rate for experimental data and numerical simulation are shown in Fig. 5 and Fig. 6 respectively. All desired parameters, updraft velocity and temperature difference increase by increasing input heat rate. For this comparison no ACW is applied in experimental and numerical model. As can be seen, there is an acceptable adoption between numerical simulation and experimental data. Due to non-ideal wall in experimental setup and existence of heat losses from collector roof, all the experimental values are slightly less than numerical results in Fig. 6.

The results of comparison between wind and no-wind conditions are shown in Fig. 7 for the vertical chimney. Ambient cross wind performed on solar collector and solar chimney causes a significant reduction in updraft velocity compared with no wind conditions. The main reason of this phenomenon is the formation of tip vortices at the chimney outlet. These vortices reduce actual cross section of chimney and make a wind induced pressure drop in the updraft flow path.

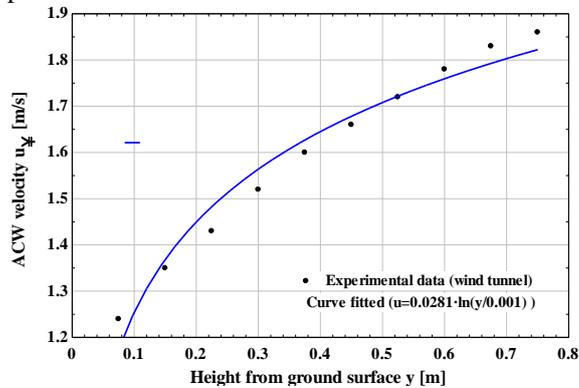


Figure 4. Ambient Cross Wind velocity profile produced by wind tunnel in experiments

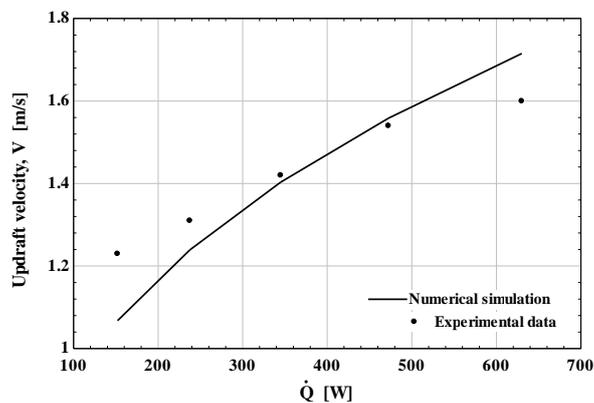


Figure 5. Variation of updraft velocity versus input heat rate with experimental data and numerical simulation

Considering Fig. 8, Collector temperature difference in windy conditions has little value due to mixing cold air entering the collector by wind and hot air generated by natural convection. Finally, Fig. 9 shows updraft velocity results for various tilt angles of the floating chimney with/without ACW. As can be seen in no-wind conditions, increase in tilt angle causes a decrease in chimney vertical height and natural convection is weakened. It is clear that, without ACW, floating chimney has no tilt angle and updraft velocity remains at 1.25 m/s for this study. For windy conditions, updraft velocity has a maximum value that occurs in a non-zero tilt angle. For this case, the angle of 10 degree has the maximum value for updraft velocity. In this region of tilt angle the effect of tip vortices and reduction of buoyancy due to reduction in vertical height will be minimum and finally solar chimney performance will reach the maximum as a result. For lower and higher values for tilt angles, a significant tip vortices effect and

reduction in driving force (buoyancy) decrease updraft velocity.

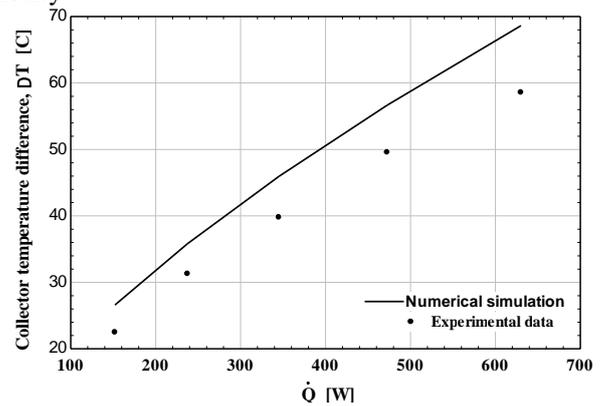


Figure 6. Variation of collector temperature difference versus input heat rate for experimental data and numerical simulation

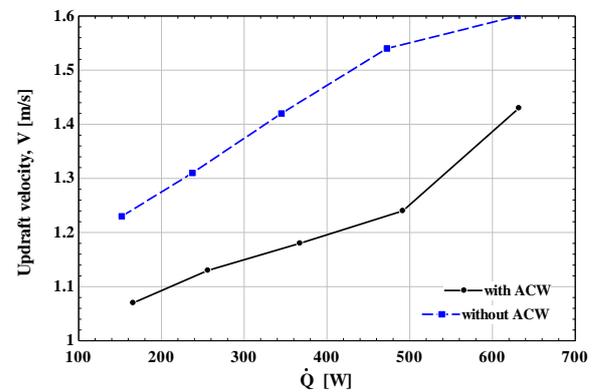


Figure 7. Comparison between updraft velocity versus input heat rate with/without ACW

## 4. Conclusions

A numerical and experimental study is investigated on ambient cross wind effect on the performance of the floating solar chimney power plant model. Updraft velocity inside the chimney and collector temperature difference were selected as the output parameters. Analysis of experimental and numerical result show that for regular week ACW velocity, updraft velocity inside the chimney and thus whole system performance will be reduced for fixed and floating chimney. Formation of tip vortices is the main reason for this deterioration and increasing of tilt angle of floating solar chimney leads to a significant improvement in system performance. The floating solar chimney has a capability to overcome the negative effect of ACW by decreasing the tip vortices within certain angles (in this study about 10 deg.) whereas fixed chimney has more problems in windy conditions. By the analysis performed in this study, some design methods can be obtained for large-scale floating chimney structure, especially for determine buoyant gas trapped in the structure and equilibrium tilt angle of chimney exposed to regular ACW. Further research on direct effects of ACW on the floating solar chimney structure is recommended.

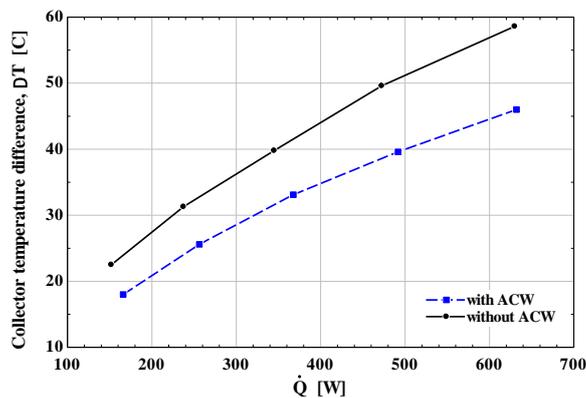


Figure 8. Comparison between collector temperature differences versus input heat rate with/without ACW

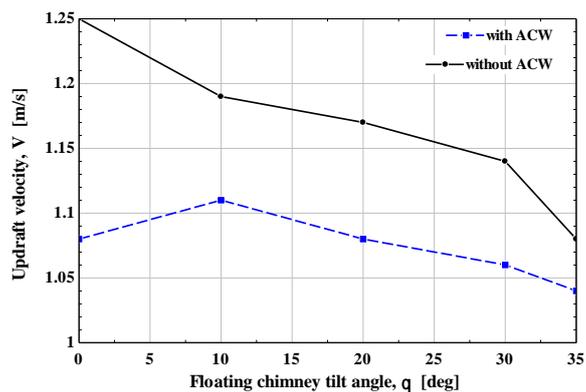


Figure 9. Variation of updraft velocity versus floating chimney tilt angle with/without ACW at constant heat flux

### Nomenclature

$C_{\epsilon 1}, C_{\epsilon 2}, C_{\epsilon 3}$  constants for turbulent model

$c_p$  specific heat at constant pressure (J/kg K)

$g$	acceleration of gravity ( $m/s^2$ )
$G$	solar radiation intensity
$Gr$	Grashof number
$G_k$	turbulence kinetic energy generation due to mean velocity gradients (J)
$G_k$	turbulence kinetic energy generation due to turbulence (J)
$L$	collector height (m)
$q$	heat flux through the ground underneath the collector ( $W/m^2$ )
$Re$	Reynolds number (dimensionless)
$T$	temperature (K)
$u$	velocity in y-direction (m/s)
$x, y, z$	Cartesian space coordinates (m/s)
$\alpha$	thermal diffusivity ( $m^2/s$ )
$\nu$	kinetic viscosity ( $m^2/s$ )
$\beta$	volume coefficient of expansion ( $1/K$ )
$\rho$	density ( $kg/m^3$ )
$\tau$	shear stress caused by viscosity ( $N/m^2$ )
Subscripts	
$s$	surface value
$i, j, k$	any direction of $x, y$ and $z$

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